Finite Element Modelling Of Thermal Processes With Phase Transitions

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Steam, Heat and Energy Production



Goal of the master's project

Finite Element Simulation to model thermal processes with phase transitions using density-enthalpy phase diagram.

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Goal of the master's project

Finite Element Simulation to model thermal processes with phase transitions using density-enthalpy phase diagram. In order to:

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Goal of the master's project

Finite Element Simulation to model thermal processes with phase transitions using density-enthalpy phase diagram. In order to: Optimize and innovate such thermal processes.

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Netherlands Organisation for Applied Scientific Research



To apply scientific knowledge with the aim of strengthening the innovative power of industry and government

Abdelhaq Abouhafç FEM Of Thermal Processes With Phase Transitions

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Outline



2 0D Boiler Simulation

3 Finite Element Method



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Density-enthalpy phase diagram



Figure: Density-enthalpy phase diagram for pure water

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0D Boiler System



Figure: Boiler

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Mass and Heat balances

$$V \frac{d\rho}{dt} = \Phi_i - \Phi_e,$$

$$V \frac{d(\rho h)}{dt} = \Phi_i \cdot h_i - \Phi_e \cdot h_e + Q + V \frac{dP}{dt}.$$

- V Volume $[m^3]$,
- ρ Density [Kg/m³],
- Φ_i Inflow mass [Kg/s],
- Φ_e Outflow mass [Kg/s],
- Q Heat flow [W],
- h Specific enthalpy [J/Kg],
- *P* Pressure [*Pa*].

Mass and Heat balances

$$\begin{split} \Phi_i &= A_i \sqrt{2\rho_i(P_i - P)}, \\ \Phi_e &= A_e \sqrt{2\rho_e(P - P_e)}, \\ Q &= AU(T_a - T). \end{split}$$

- A_i Inlet area $[m^2]$,
- A_e Exit area $[m^2]$,
- T_a Ambient temperature [K],
- U Heat transfer coefficient $[W/m^2/K]$.

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Dry Boiling



Figure: Level, Temperature and Pressure. $A_i << A_e, P_i = 10$ bar, $P_e = 1$ bar, $T_a = 500K$

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Over flow



Figure: Level, Temperature and Pressure. $A_i >> A_e, P_i = 10$ bar, $P_e = 1$ bar, $T_a = 400K$

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Poisson Equation

Poisson equation in one dimension

$$\begin{aligned} -k\frac{d^2T}{dx^2} &= f(x), \quad 0 \le x \le \pi \\ T(0) &= 0, \\ \frac{dT}{dx}(\pi) &= 0. \end{aligned}$$

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Weak Formulation

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• Multiplying by a test function η , satisfying: $\eta(0) = 0$ $\int_0^{\pi} \left(k \frac{d^2 T}{dx^2} + f \right) \eta dx = 0,$

$$-\int_0^{\pi} k \frac{d\eta}{dx} \frac{dT}{dx} d\Omega + \int_0^{\pi} \eta f d\Omega + \left[\eta(k \frac{dT}{dx})\right]_0^{\pi} = 0,$$

Application of BC, $\frac{dT}{dx}(\pi) = 0$ and $\eta(0) = 0$
$$\int_0^{\pi} k \frac{d\eta}{dx} \frac{dT}{dx} d\Omega = \int_0^{\pi} \eta f d\Omega.$$

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Galerkin Approximation

Galerkin Equations

$$\sum_{j=1}^{n} \int_{0}^{\pi} k \frac{d\varphi_{i}}{dx} \frac{d\varphi_{j}}{dx} d\Omega = \int_{0}^{\pi} f\varphi_{i} d\Omega, \quad i = 1, ..., n.$$

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Matrix Form

$$ST = F$$
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Stiffness Matrix

$$S_{ij} = \int_0^\pi k \frac{d\varphi_j}{dx} \frac{d\varphi_i}{dx} dx,$$

vector F

$$F_i = \int_0^\pi f \varphi_i dx.$$

Numerical Solution

If f(x) = sin(x), then the exact solution is $T(x) = \frac{1}{k}sin(x) + \frac{x}{k}$



Figure: Exact and Numerical Solution of 1D Poisson Equation, k = 0.1

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2D Convection Diffusion Equation

$$\frac{\partial T}{\partial t} - \vec{\nabla} \cdot \left(k \vec{\nabla} T \right) + \left(\vec{u} \cdot \vec{\nabla} T \right) = f$$

- k diffusion term,
- u convection term,
- f source term.

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Numerical Solution



On the boundary $B1 \cup B4$: On the boundary $B2 \cup B3$: At the starting time t_0 :

$$T|_{B1\cup B4} = 20,$$

$$k\frac{\partial T}{\partial n}|_{B2\cup B3} = 0,$$

$$T|_{t_0} = 20.$$

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Standard Galerkin Method



Figure: Numerical solution of 2D time dependent convection diffusion equation using SGA method and implicit scheme, dt = 0.1

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Numerical Solution



On the boundary $B1 \cup B3$: $k\frac{\partial}{\partial}$ On the boundary B4: $T|_{L}$ On the boundary B2: $T|_{L}$ At the starting time t_0 : $T|_{t}$

$$k \frac{\partial T}{\partial n}|_{B1\cup B3} = 0,$$

 $T|_{B4} = 20,$
 $T|_{B2} = 40,$
 $T|_{t_0} = 20.$

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Standard Galerkin Method



Figure: Numerical solution of 2D time dependent convection diffusion equation using SGA method and implicit scheme after 500 time steps, dt = 0.1

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Streamline Upwind Petrov Galerkin Method



Figure: Numerical solution of 2D time dependent convection diffusion equation using SUPG method and implicit scheme after 500 time steps, dt = 0.1

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Further Research



Inert and liquid Inert, liquid and gas Inert and gas

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Figure: Porous media

1D Porous media

Solve two coupled nonlinear PDE:

$$\frac{\partial \rho}{\partial t} - \frac{K}{\mu} \frac{\partial P}{\partial x} \frac{\partial \rho}{\partial x} = \rho \frac{\partial}{\partial x} \frac{K}{\mu} \frac{\partial P}{\partial x},$$
$$\rho \frac{\partial h}{\partial t} - \frac{\partial P}{\partial t} - \rho \frac{K}{\mu} \frac{\partial P}{\partial x} \frac{\partial h}{\partial x} = \frac{\partial}{\partial x} \lambda \frac{\partial T}{\partial x} + q.$$

Initial and boundary conditions:

$$P|_{t_0} = P_a,$$

$$T|_{t_0} = T_a,$$

$$\frac{K}{\mu} \frac{\partial P}{\partial x} = k_m (P_a - P),$$

$$\lambda \frac{\partial T}{\partial x} = k_h (T_a - T).$$

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1D Porous media

where:

- t_0 starting time [s],
- λ heat conductance coefficient [W/m/K],
- μ dynamic viscosity [*Pa.s*],
- ρ density [Kg/m³],
- K permeability [Darcy],
- k_h heat transfer coefficient $[W/m^2/K]$,
- k_m mass transfer coefficient $[Kg/m^2/K]$.

Further Research

- Set up 1D model for porous system and solve it using MATLAB.
- Set up 2D and 3D model for porous system and solve them using SEPRAN.

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Questions



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