# Finite Element Modelling Of Thermal Processes With Phase Transitions

Abdelhaq Abouhafç

Delft University of Technology TNO Science and Industry

June 14, 2007

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#### Introduction: Boiler System



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# Aim and Difficulties

#### Aim:

Finite Element modelling of thermal processes with phase transitions using density-enthalpy phase diagrams

#### Difficulties:

- Nonlinearity
- Time dependent problem
- Coupled equations
- High convection: Numerical oscillations
- Accuracy and stability



#### Classical methods versus Density Enthalpy method

2 Mathematical Model

- 3 Numerical Results
- 4 2D FEM Modelling of Boiler System
- **5** Conclusions and Recommendations

### Classical methods: Disadvantages

- For each phase: a set of equations
- A lot of coefficients and parameters
- Discontinuity across the interfaces
- A lot of assumptions: Less accurate

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# Density Enthalpy method: Advantages

- One set of equations
- Less input parameters
- Less assumptions
- Accuracy
- Stability

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# Density-Enthalpy phase diagrams: $T = T(\rho, h), P = P(\rho, h).$



Figure: Temperature and Pressure as functions of density and enthalpy for pure water

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# Density-Enthalpy phase diagram: $X^{G} = X^{G}(\rho, h)$ .



Figure: Gas Mass fraction as function of density and enthalpy for pure water

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# Mass and Energy balances

$$\begin{array}{rcl} \frac{\partial \rho}{\partial t} &=& -\vec{\nabla}.\left(\rho\vec{v}\right)\\ \frac{\partial(\rho h)}{\partial t} &=& -\vec{\nabla}.\left(\rho h\vec{v}\right) + \vec{\nabla}.\left(\lambda\vec{\nabla}T\right) + q \end{array}$$

- ho density [Kg/m<sup>3</sup>]
- h enthalpy  $[Kg/m^3]$
- T temperature [K]
- $\vec{v}$  velocity [m/s]
- $\lambda$  heat conduction [W/m/K]
- q heat source  $[W/m^3]$

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$$\vec{\mathbf{v}} = -\frac{K}{\mu}\vec{\nabla}P$$

- $\vec{v}$  velocity [m/s]
- K permeability  $[m^2]$
- $\mu$  dynamic viscosity [*Pa.s*]
- P pressure [Pa]

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# **Boundary Conditions**

The external mass transfer:

$$\rho \vec{\mathbf{v}}.\vec{\mathbf{n}} = k_m \left(\rho - \rho_a\right)$$

- $k_m$  mass transfer coefficient [m/s]
- $\rho_a$  ambient density  $[Kg/m^3]$

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# **Boundary Conditions**

#### External Energy transfer by convection:

• if 
$$\rho - \rho_a > 0$$
  
( $\rho h$ )  $\vec{v} \cdot \vec{n} = h|_{\Gamma} k_m (\rho - \rho_a)$   
• if  $\rho - \rho_a < 0$   
( $\rho h$ )  $\vec{v} \cdot \vec{n} = h_a k_m (\rho - \rho_a)$ 

External energy transfer by conduction:

$$\lambda \vec{\nabla} T.\vec{n} = k_h \left( T - T_a \right)$$

 $k_h$  heat transfer coefficient  $[W/m^2/K]$  $h_a$  ambient enthalpy [J/Kg]

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## **Initial Conditions**

$$\begin{array}{lll} \rho(t_0,x) &=& \rho_0, \quad x\in\Omega,\\ h(t_0,x) &=& h_0, \quad x\in\Omega. \end{array}$$

- $\Omega$  domain
- $t_0$  starting time [s]

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# Numerical Approach: transform PDEs to ODEs

• Weak formulation:

$$\int_{\Omega} \frac{\partial \rho}{\partial t} \eta dV = - \int_{\Omega} \vec{\nabla} . \left( \rho \vec{v} \right) \eta dV$$

Integration by parts:

$$\int_{\Omega} \frac{\partial \rho}{\partial t} \eta dV = -\int_{\Gamma} \rho \eta \vec{v}.\vec{n} dS + \int_{\Omega} \rho \vec{v}.\vec{\nabla} \eta dV$$

- $\Omega$  domain
- Γ boundary
- $\vec{n}$  outward unit normal to  $\Gamma = \partial \Omega$
- $\eta$  test function

# Numerical Approach: transform PDEs to ODEs

• Use the boundary conditions:

$$\int_{\Omega} \frac{\partial \rho}{\partial t} \eta dV = \int_{\Gamma} \eta k_m \left( \rho_a - \rho \right) dS - \int_{\Omega} \rho \frac{K}{\mu} \vec{\nabla} P . \vec{\nabla} \eta dV$$

• The solution  $\rho(\vec{x}, t)$  is approximated by:

$$ho(ec{x},t) = \sum_{j=0}^N 
ho_j(t) arphi_j(ec{x})$$

- $\rho_j$  unknown density
- $\varphi_j$  basis function
- N + 1 number of mesh nodes for the unknowns

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## Numerical Approach: transform PDEs to ODEs

• Galerkin approximation:

$$\sum_{j=0}^{N} \frac{d\rho_j(t)}{dt} \left( \int_{\Omega} \varphi_i \varphi_j dV \right) = \int_{\Gamma} \varphi_i k_m \left( \rho_a - \sum_{j=0}^{N} \rho_j(t) \varphi_j \right) dS - \sum_{j=0}^{N} \left( \int_{\Omega} \frac{K}{\mu} \vec{\nabla} P. \vec{\nabla} \varphi_i \varphi_j dV \right) \rho_j(t)$$

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# Numerical Approach: transform PDEs to ODEs

• System of nonlinear ODEs:

$$M\frac{d\vec{\rho}}{dt} = S(\vec{\rho},\vec{h})\vec{\rho} + \vec{F}$$

- $\vec{
  ho}$  unknown density
- M mass Matrix
- S stiffness Matrix
- $\vec{F}$  vector

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- Use SUPG method to reduce the effect of high convection,
- Use Implicit backward Euler scheme to guarantee stability.

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## Types of simulated systems



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### Open System to Mass, $k_m = 2, k_h = 0, dt = 0.001$



Figure: Density and Total Enthalpy after 5000 time steps

#### Open System to Mass, $k_m = 2, k_h = 0, dt = 0.001$



Figure: Temperature and Pressure after 5000 time steps

## Open System to Mass, $k_m = 2, k_h = 0, dt = 0.001$



Figure: Gas Mass Fraction, Total Mass and Energy after 5000 time steps

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### Thermodynamical results

- Density inside an open system to mass, tends to the ambient density when the system reaches its steady state,
- The external transfer process of mass and energy stops as soon as the system reaches its steady state at thermodynamical equilibrium.

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# Geometry and Operating Conditions



# 2D Boiler: Mass is flowing out and Energy is flowing in



Figure: Density and Total Enthalpy with respect to x and y after 200000 time steps, dt = 0.001

# 2D Boiler: Mass is flowing out and Energy is flowing in



Figure: Temperature and pressure with respect to x and y after 200000 time steps, dt = 0.001

# 2D Boiler: Mass is flowing out and Energy is flowing in



Figure: Gas Mass Fraction with respect to x and y after 200000 time steps, dt = 0.001



- Set up a stable and accurate FEM model using Density-Enthalpy diagrams (0D, 1D and 2D with Matlab),
- Output: Numerical results are logical and have obtained for problems where classical methods may not work.

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# Recommendations

- Transfer model to SEPRAN,
- Study more aspects of the model (Compare implicit with explicit),
- Exploit the sparsity of the matrix: essential for saving memory and computing time,
- Apply iterative solvers to speed up calculations,
- Validation of the numerical model: Compare with experimental results,
- Add the gravity force to the equations.

#### Questions



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